



# Synthesis of Zeolite using Fly ash and its application in Removal of $\text{Cu}^{2+}$ , $\text{Ni}^{2+}$ , $\text{Mn}^{2+}$ from Paper Industry Effluent

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Available online at: [www.isca.in](http://www.isca.in), [www.isca.me](http://www.isca.me)

Received 2<sup>nd</sup> January 2014, revised 16<sup>th</sup> February 2014, accepted 15<sup>th</sup> March 2014

## Abstract

An improved synthesis for fly ash based zeolite has been attempted and studies have been carried out for the removal of  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$  and  $\text{Mn}^{2+}$  from paper industry wastewater. The parameters affecting adsorption process, such as initial pH, weight of zeolite, contact time were investigated. The transition metal ions present in the waste  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$  and  $\text{Mn}^{2+}$  shows better adsorption capacities on synthesized zeolite. The order of removal of heavy metal ions is  $\text{Ni}^{2+} > \text{Mn}^{2+} > \text{Cu}^{2+}$ .

**Keywords:** Fly ash, zeolite, paper industry waste, transition metal ions, adsorption, atomic absorption spectrophotometer.

## Introduction

Wastewater from various industries such as electroplating, paper and pulp, metal plating, mining operations, battery manufacturing processes, glass production processes are known to contain heavy metals such as Cu, Ni, Pb, Cr, Zn, Cd and Fe. These heavy metals are non-biodegradable which leads to several health problems in animals, plants and human beings such as cancer, kidney failure, metabolic acidosis, oral ulcer, renal failure and damage in stomach of the rodent<sup>1</sup>. These contaminants must be removed from wastewaters before discharge as they are considered persistent, bio accumulative and toxic substances<sup>2</sup>. Among the advanced methods of heavy metal removal, adsorption is the most effective and economical because of their relative low cost<sup>3</sup>.

In India nearly 90 mt of fly ash is generated per annum and is responsible for environmental pollution<sup>4</sup>. The bulk of fly ash is stored in ash dams and landfills. The ash dams are costly to manage, lead to loss of usable land, impact negatively on the environment, cause air and water pollution. Fly ash is primarily composed of aluminosilicate glass, mullite ( $\text{Al}_6\text{Si}_2\text{O}_{13}$ ) and quartz ( $\text{SiO}_2$ ). Low Si / Al ratio zeolite provides an excellent sorbents for the adsorption of transition metals due to high cation exchange capacities (CEC) and large pore volumes<sup>5,6</sup>. The water pollution in Kanhan river caused due to the disposal of waste from Khaperkheda thermal power station was studied<sup>7</sup>. Fly ash based zeolite shows higher adsorption capacity for the removal of  $\text{Cu}^{2+}$ ,  $\text{Pb}^{2+}$  and  $\text{Cd}^{2+}$  from waste water than that of fly ash<sup>8</sup>. It is reported that Na-P1, hydroxysodalite and X-type zeolites synthesized from fly ash are effective in removing Fe, Cu, Zn and Pb from the contaminated effluent streams<sup>9-11</sup>. Among natural zeolites, chitosan, a biopolymer has been studied as a low cost adsorbent for the removal of lead from waste water<sup>12</sup>.

Zeolite – A obtained from fly ash (FAZ – A) has been patented nationally and internationally. FAZ –A shows maximum efficiency for lead removal followed by cadmium and copper<sup>13</sup>.

The objective of this is to develop an improved synthesis of zeolite from fly ash and find its application in the removal of heavy metal ions from paper industrial effluents. Since the existing methodologies have mostly used NaOH and  $\text{Na}_2\text{CO}_3$  for hydrothermal synthesis of zeolite from fly ash, we thought of studying the effect of addition of KOH to NaOH and  $\text{Na}_2\text{CO}_3$ . Experiments were carried out to demonstrate the heavy metal removal efficiency of this newly synthesized zeolite from paper industry waste water.

## Material and Methods

**Material Handling and storage:** Pulverized coal fly ash obtained from Khaperkheda Thermal Power Station was used as a raw material. Fresh fly ash samples were collected from precipitators and stored in sealed plastic container having an airtight lid. The plastic containers were stored in a dark cool room away from the sources of moisture, direct sunlight and from fluctuating temperatures<sup>14</sup>.

Paper industry waste water was collected from the industry in Maharashtra Industrial Development Corporation (MIDC), Nagpur. Sampling was carried out by following the standard procedures and techniques<sup>15</sup>.

After the collection of sample, parameters such as temperature, pH and colour are measured by using thermometer, pH meter and by visual observation. Then the sample was transferred to Amber Coloured glass bottle in order to prevent oxidation of metal ions. Fly ash characterization was done by X-ray fluorescence at Indian Bureau of Mines (IBM), MIDC, Nagpur.

Analysis of paper industrial waste was carried out by atomic absorption spectrophotometer (AAS) (GBC 906 AA) and inductively coupled plasma spectrometer (ICP) (GY 166 Ultrace)<sup>16</sup> from IBM, MIDC, Nagpur. Analysis revealed presence of  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Mn}^{2+}$ ,  $\text{Cr}^{6+}$  and  $\text{Fe}^{3+}$ . In this work, we have studied the removal of  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$  and  $\text{Mn}^{2+}$  by using newly synthesized zeolite as adsorbent.

**Zeolite Synthesis:** The fly ash was initially screened to eliminate larger particles by using Mechanical Sieve Shaker (Filterwel test sieves) of mesh size 72  $\mu$ . Fly ash was subjected to pretreatment with 8N HCl for 2 hours. Fusion of fly ash with NaOH and  $\text{Na}_2\text{CO}_3$  was done at the ratio of 1: 1.5: 0.5. KOH (0.1g) was added to it and the mixture was heated in muffle furnace at 700°C for 1 hour. Fused mass was cooled, milled and mixed thoroughly in distilled water with simultaneous addition of sodium aluminate solution. The slurry so obtained was then subjected to stirring and ageing for 8 – 10 hours. It was then subjected to hydrothermal crystallisation in a closed container in an oven at 100°C for 2 – 3 hours. After crystallisation the solid crystalline product was recovered by filtration using vacuum pump. It was washed with double distilled water and dried in oven. The steps after fusion were followed as mentioned in literature<sup>17</sup>.

The efficiency of this newly synthesized zeolite as adsorbent for the removal of heavy metal ions from the industrial waste was studied as follows.

**Adsorption Experiments:** Batch mode experiments were performed in 100 ml conical flasks by addition of desired amount of zeolite to 50 ml of waste water. In all experiments, the flasks were shaken at 100 rpm on the mechanical shaker for predetermined time intervals at temperatures 25°C. After agitation the zeolite was separated by filtration and some aliquots of filtrate in the supernatant were analysed using atomic adsorption spectrophotometer (AAS) and inductively coupled plasma spectrophotometer (ICP). The amount of metal ion adsorbed on the zeolite was computed by the following equation:

$$\% \text{ removal} = (\text{Ci} - \text{Ce})/\text{Ci} * 100$$

Where  $\text{Ci}$  = Concentration before adsorption,  $\text{Ce}$  = Concentration after adsorption.

The pH of the solution was found to be 5. The effect of weight of zeolite on removal of transition metal ions was studied by adding 50 ml of waste water to the 0.1g, 0.2g, 0.3g, 0.4g and 0.5g of zeolite in conical flasks. The mixtures were shaken in a mechanical shaker at about 100 rpm for 5 hours. The filtrate was analysed by using atomic adsorption spectrophotometer (AAS) and inductively coupled plasma spectrophotometer (ICP). To the 50 ml of industrial waste water 0.1g of zeolite was mixed in order to investigate the effect of contact time on adsorption of transition metal ions. The flasks were shaken for 1, 2, 3, 4 and 5 hrs. The concentration of metal ions was obtained by using AAS and ICP. Similarly the effect of pH on adsorption of transition metal ions was studied by adjusting the pH of the industrial waste water to 1, 2, 3, 4 and 5 by adding HCl. The solutions were treated as previously and analysed using AAS and ICP.

## Results and Discussion

**Characterisation of zeolite synthesized from fly ash:** The results of the elemental composition of zeolitic material was analysed by Energy Dispersive X-ray Fluorescence (EDXR) (Model no.EDX700, Shimadzu) and presented in table 1.

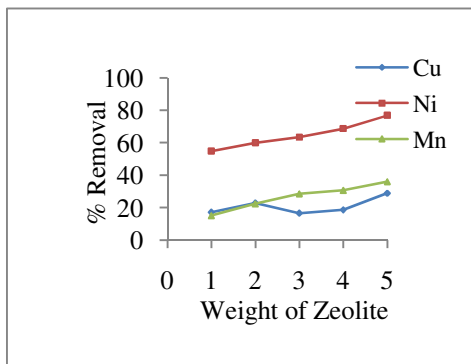
**Adsorption Experiments: Effect of weight of zeolite, contact time and pH on sorption of ions  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Mn}^{2+}$ :** The effect of adsorbent doses on the removal of transition metal ions  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Mn}^{2+}$  is shown in figure 1. The amount of sorbent was varied from 0.1 to 0.5 g/L and equilibrated for 5 hrs. The results indicated that the percent removal of  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$  and  $\text{Mn}^{2+}$  decreases with the increase in adsorbent dose and was maximum 54.51% at 0.1 g/L of zeolite.

The equilibrium time required for the sorption of transition metal ions  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$  and  $\text{Mn}^{2+}$  on the zeolite with 0.1 g/L at different time intervals was studied. Figure 2 showed that adsorption capacity sharply increased with increase in time and attains equilibrium in 5 hrs. Therefore, the adsorption time was set to 5 hrs. in each experiment. The order of adsorption of transition metal ions on zeolite was  $\text{Ni}^{2+} > \text{Mn}^{2+} > \text{Cu}^{2+}$ .

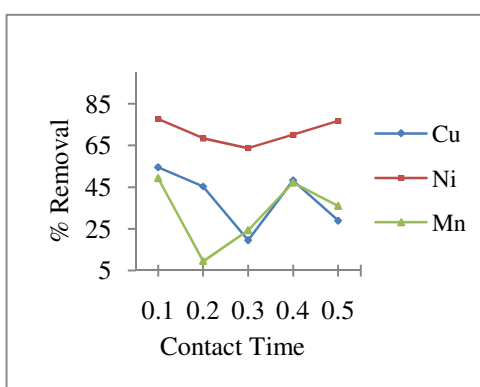
Aqueous phase pH governs the speciation of metals and also the dissociation of active functional sites on the sorbent. Hence metal sorption is critically linked with pH<sup>18</sup>. In order to establish the effect of pH on the adsorption of  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$  and  $\text{Mn}^{2+}$  onto the synthesized zeolite, batch sorption studies at different values of pH were conducted in the range of 1 to 5 (figure 3). It was observed that the maximum adsorption of transition metal ions was observed at pH 5.

**Table-1**  
**EDXR of synthesized Zeolite**

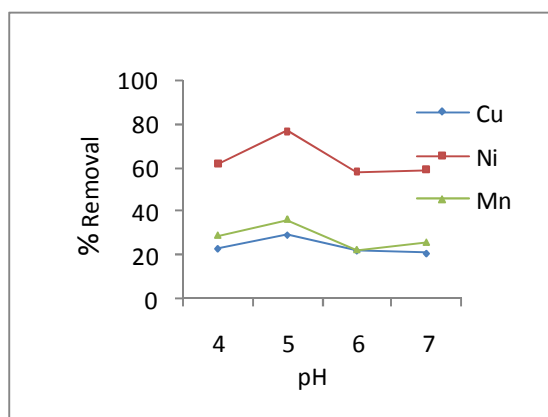
	$\text{Al}_2\text{O}_3$	$\text{SiO}_2$	$\text{Na}_2\text{O}$	$\text{MgO}$	$\text{K}_2\text{O}$	$\text{CaO}$	$\text{Fe}_2\text{O}_3$	$\text{TiO}_2$	$\text{Mn}_2\text{O}_3$	$\text{NiO}$	$\text{CuO}$	$\text{SrO}$	$\text{ZrO}_2$	$\text{BaO}$
Mass %	41.22	46.22	0.75	0.205	0.902	3.621	2.254	0.826	3.036	0.171	0.353	0.125	0.216	0.101



**Figure-1**  
Effect of weight of zeolite on sorption



**Figure-2**  
Effect of contact time on sorption



**Figure-3**  
Effect of pH on sorption on metal ions

**Adsorption Isotherms:** The Langmuir isotherm model is the most common model used to quantify the amount of adsorbate adsorbed on an adsorbent. The Langmuir isotherm can be expressed in terms of a dimensionless constant  $R_L$ , is defined as

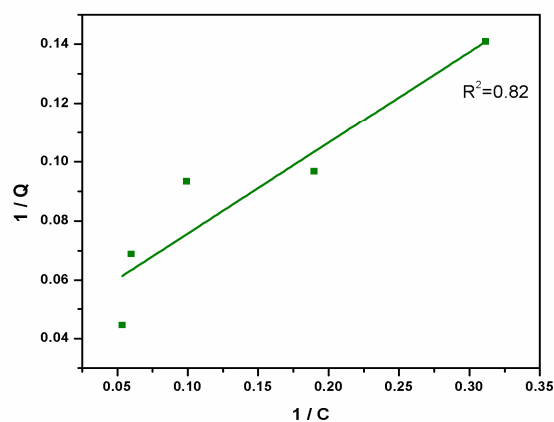
$$R_L = 1 / (1 + K_A C_0)$$

Where  $C_0$  is the initial concentration (mg/l),  $R_L$  indicates the isotherm,  $K_A$  is the rate of adsorption. The values of  $R_L$  were found to be in between 0 to 1, which indicates favourable adsorption of metals under study onto the adsorbent<sup>19</sup>.

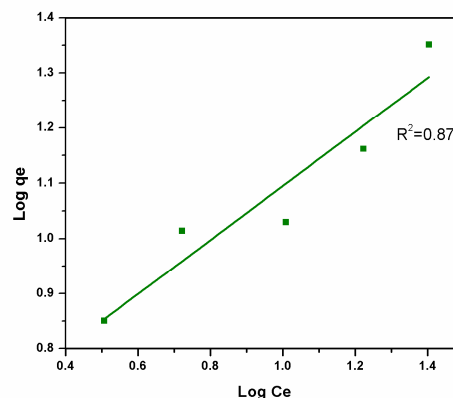
The liberalized Freundlich model isotherm was applied for the adsorption of heavy metal ions and is expressed as  $\text{Log}(X/m) = \text{Log } K_F + 1/n (\text{Log } C_e)$

Where,  $(x/m)$  is the amount of heavy metal ions adsorbed at equilibrium (mg/g),  $C_e$  is the equilibrium concentration of heavy metal ions (mg/l).  $K_F$  and  $n$  are the constants values calculated from the intercept and slope of the plot.

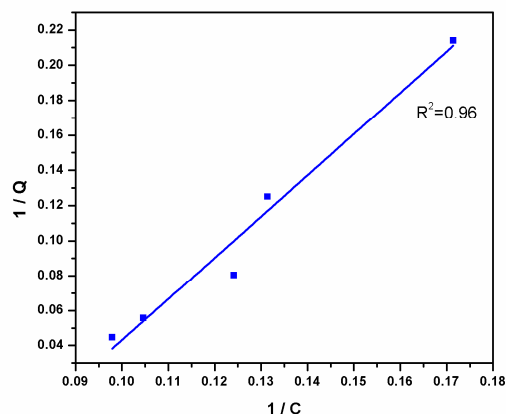
The regression coefficient  $R^2$  for Langmuir and Freundlich values for  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Mn}^{2+}$  adsorption were found to be between 0 to 1 indicating favourable adsorption of the metal ions onto the synthesized zeolite. The function of the strength of adsorption in the adsorption process,  $1/n$  for Ni adsorption was found to be above 1, which indicates co-operative adsorption<sup>20</sup>.



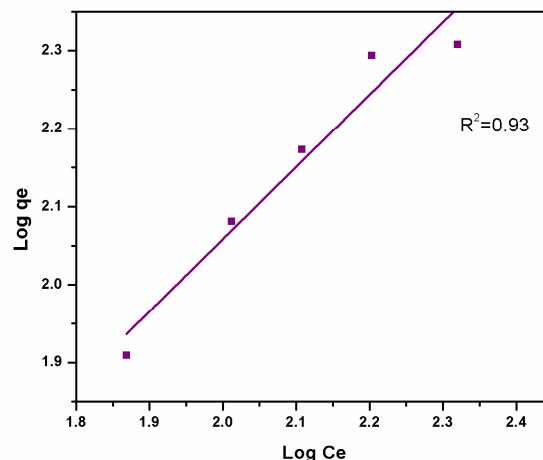
**Figure-4**  
Langmuir isotherm for  $\text{Cu}^{2+}$



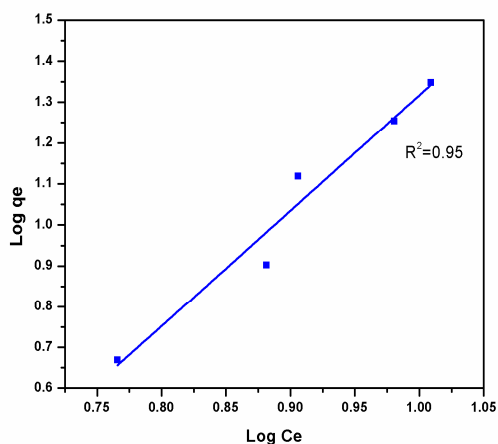
**Figure-5**  
Freundlich isotherm for  $\text{Cu}^{2+}$



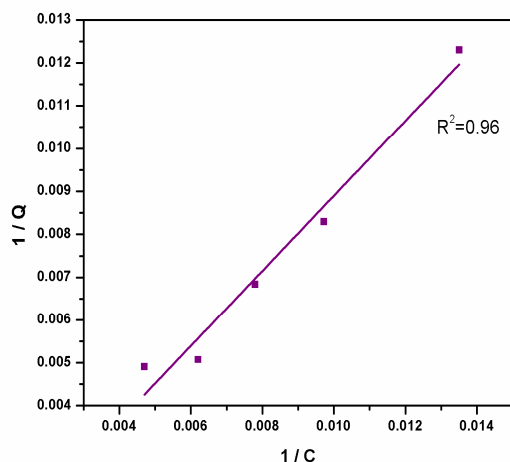
**Figure-6**  
Langmuir isotherm for  $\text{Ni}^{2+}$



**Figure-9**  
Freundlich isotherm For  $\text{Mn}^{2+}$



**Figure-7**  
Freundlich isotherm for  $\text{Ni}^{2+}$



**Figure-8**  
Langmuir isotherm For  $\text{Mn}^{2+}$

## Conclusion

Zeolite – P have been prepared from coal combustion fly ash by a hydrothermal treatment of the ash with NaOH,  $\text{Na}_2\text{CO}_3$  and KOH. By varying the fusion ratio zeolite – P was achieved. The resultant zeolite – P was more effective in the removal of transition metal ions present in the paper industry effluent. The order of removal of heavy metal ions was  $\text{Ni}^{2+} > \text{Mn}^{2+} > \text{Cu}^{2+}$ .

It is envisaged that this modification procedure can convert fly ash into a beneficial product which would prove effective in removing transition metal ions from paper industrial waste water.

## Acknowledgement

The authors are thankful to University Grants Commission for providing support to our research activities.

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