

Short Communication

Chitosan for the Removal of Chromium from Waste Water

Singh Dhanesh¹ and Singh Anjali²

¹Deptt. of chemistry, K.G. Arts and Science College, Raigarh, C.G, INDIA

²School of Applied and Social Sciences, Singhania University, Pacheri Bari, Jhunjhunu, Raj, INDIA

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Abstract

The sorption of chromium (VI) on chitosan has been found to be dependent on contact time, concentration, temperature, and pH of the solution. The process of removal follows first order kinetics and absorption of heat.

Keywords: Chitosan, bioabsorbent, chromium (VI), heavy metal adsorption, Chitin

Introduction

The general methods of treating wastewater having chromium follow precipitation and ion exchange¹. Recently, much interest has been exhibited in the use of sorption technique for the removal of cadmium from wastewater using chitosan. The present investigation aims at using chitosan, a low cost and highly effective sorbent for the removal of cadmium from waste water. Chitosan is a biopolymer, which is extracted from crustacean shells or from fungal biomass². The structure of chitosan is presented schematically in figure-1

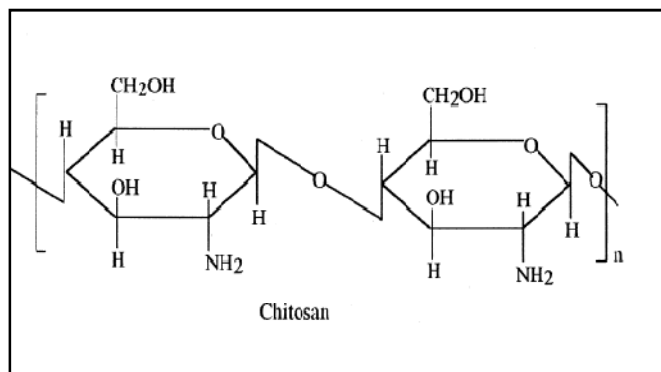


Figure-1
Structure of chitosan

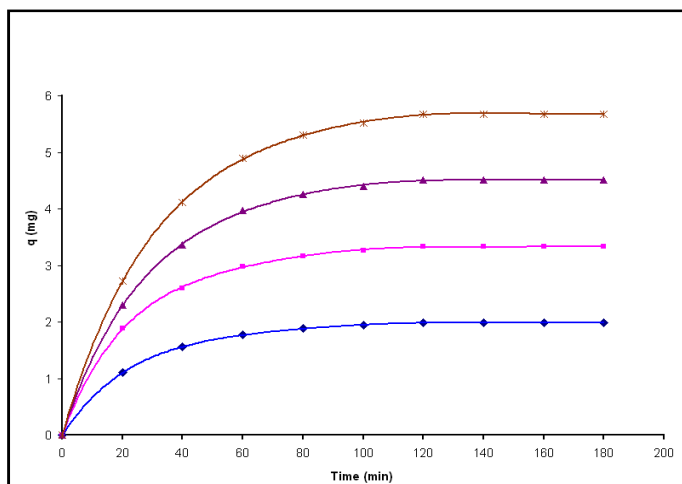
Material and Methods

Experimental Procedure: Chitosan was obtained from India sea foods, cochi India. Batch sorption experiments were carried out in temperature controlled shaking machine by agitating 25ml aqueous solutions of sorbates with 1.0 g sorbent in different glass bottles at different conditions of concentrations, temperatures and pH. The pH of different solutions was adjusted with 0.05 M NaOH or HCl by pH meter, systronic 335. The speed of agitation was maintained at 1000 rpm to ensure equal mixing. The progress of sorption was noted after each 20 min

till saturation. At the end of predetermined time interval each 20 min, the sorbate and sorbent were separated by centrifugation at 16,000 rpm and the supernatant liquid analyzed by atomic absorption spectrophotometer.

Results and Discussion

Effect of Contact Time and Concentration: The removal of Cr (VI) by sorption on chitosan from aqueous solution increase with time (figure-2) till equilibrium is attained in 140 min. The figure show that time of saturation is independent of concentration. It is further noted that the amount of Cr (VI) sorbed increases from 1.960 mg.g⁻¹ to 5.701 mg.g⁻¹ by increasing Cr (VI) concentration from 100 mg/l to 250 mg/l. the time-amount sorbed curve is single, smooth and continuous indicating monolayer coverage of Cr (VI) on the outer surface of chitosan³.



Figur-2
Effect of concentration for the sorption of chromium (VI) on chitosan;
● 100 mg/L, ■ 150 mg/L, ▲ 200 mg/L, * 250 mg/L

Sorption Kinetics: The kinetics of sorption of Cr (VI) on chitosan was studied using Lagergren equation⁴,
 $\text{Log}(q_e - q) = \text{log } q_e - kt / 2.3 (1)$

Where q_e and q are the amount sorbed (mg.g^{-1}) of Cr (VI) at equilibrium and at time 't' respectively and k is sorption constant. The straight lines obtained from the plots of $\text{log}(q_e - q)$ against 't' (figure-3) and different concentrations indicate that the sorption process follows first order kinetics.

Effect of Temperature: The amount of Cr (VI) sorbed on chitosan increases from 1.987 mg.g^{-1} to 2.488 mg.g^{-1} by increasing temperature from 30°C to 40°C indicating the process to be endothermic (figure-4).

Langmuir Isotherm: The equilibrium data at the different temperatures follow Langmuir equation⁵,
 $C_e/q_e = 1/\phi.b + C_e/\phi (2)$

Where $C_e \text{ mg.L}^{-1}$ is equilibrium concentration of Cr (VI) and ϕ and b are Langmuir constants related to sorption capacity and sorption energy respectively. The value of ϕ and b (table 4) were determined from the slope and intercept of linear plots figure-5. The sorption capacity also increases with 0 temperature suggesting that the active centers available for sorption have increased with temperature.

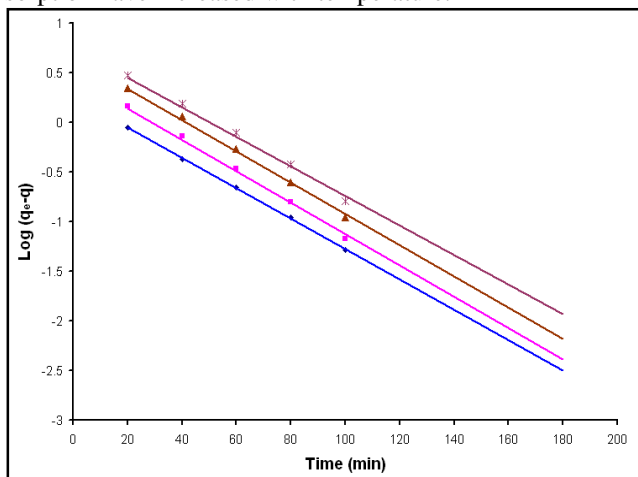


Figure-3

**Lagergren plot for the sorption of Cr (VI) on chitosan;
 ● 100 mg/L, ■ 150 mg/L, ▲ 200 mg/L, * 250 mg/L, pH 5,
 temp 30°C**

The change in free energy (ΔG°), enthalpy (ΔH°), and entropy (ΔS°) of sorption have been calculated using following equations,

$$\Delta G^\circ = -RT \ln K \quad (3)$$

$$\Delta H^\circ = RT_1 T_2 (T_1 - T_2) \ln k_2 / k_1 \quad (4)$$

$$\Delta S^\circ = \Delta H^\circ - \Delta G^\circ / T_1 \quad (5)$$

Where K_1 and K_2 are equilibrium constants at temperature T_1 and T_2 respectively. The negative values of ΔG° (table 2)

indicate the spontaneous nature of the sorption process. The positive values of ΔH° at different temperature support the endothermic nature of the process⁶.

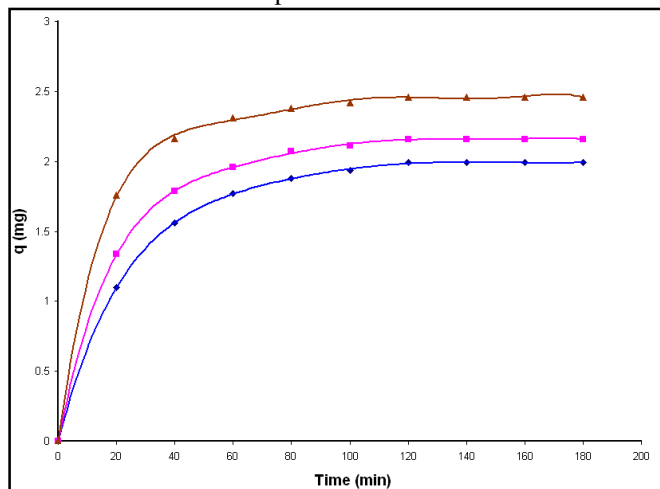


Figure-4

**Effect of temp. On the sorption of Cr (VI) on Chitosan ●
 30°C, ■ 40°C, ▲ 50°C**

Table-1

Ø Values at Different Temp and pH

Temperature ($^\circ\text{C}$)	Ø mg.g^{-1}	p ^H	Ø mg.g^{-1}
30	0.4718	2	0.0155
40	0.4439	4	0.0153
50	0.3927	6.5	0.0137

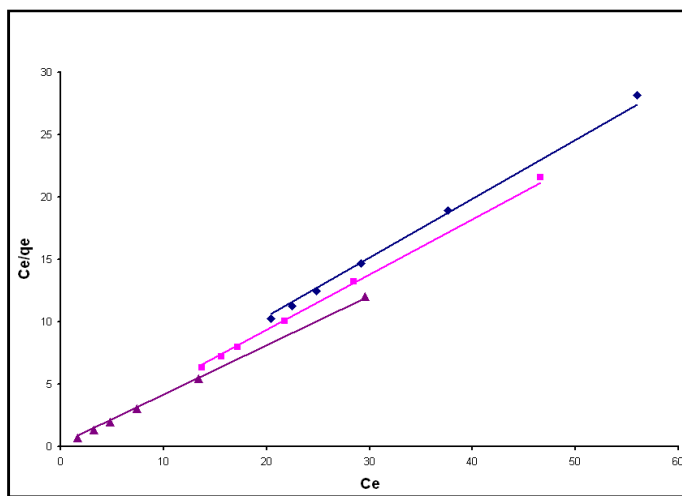


Figure-5

**Langmuir isotherm for the sorption of Cr (VI) on chitosan;
 ● 30°C, ■ 40°C, ▲ 50°C.**

Effect of pH: The amount of Cr (VI) sorbed on chitosan decreases from 2.298 mg.g^{-1} (91.92 %) to 1.598 mg.g^{-1} (63.92 %) by increasing pH of the solution from 2.0 to 6.5 (figure-5). The Sorption capacity ϕ , also decrease with the increase of pH⁷.

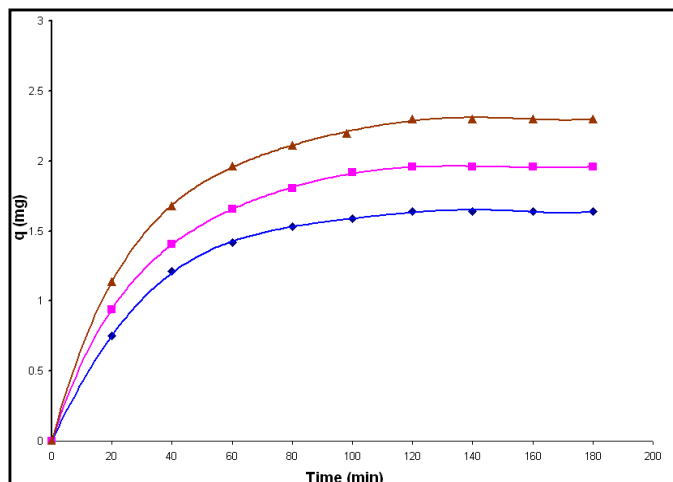


Figure-7

Effect of pH on the sorption of chitosan; ●2.0, ■ 4.0, ▲6.5;
temp: 30 ° C, conc. 100 mg/l

Table-2

Thermodynamic parameters at different temperatures

Temperature (°C)	ΔG° (kcal.mol ⁻¹)	ΔH° (kcal.mol ⁻¹)	ΔS° (kcal.mol ⁻¹)
30	-17.110	11.37	0.191
40	-25.27	28.10	0.708
50	-37.87		

Conclusion

From the above discussion it is clear that due to chemical composition, structure, more adsorption sites, cheap, availability in plenty etc. this substance will provide to be efficient adsorbent.

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